



제 1 강

부록 **A1** : 물리학 배경지식

제 1 장 : 서론

삼성중공업 계약학과 선체저항

2013년도 봄학기

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담당교수 : 이 인 원

Fluid Mechanics ?

- **Everything flows, nothing stand still.**

- Heraclitus (Greek Philosopher, 535 ~ 475 B.C.)

- 다음 방정식은 같은가, 다른가?

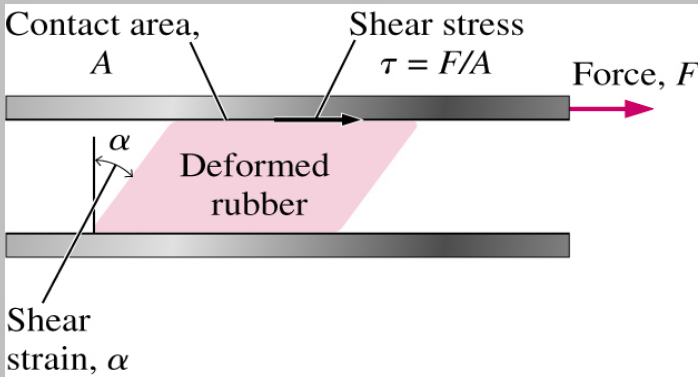
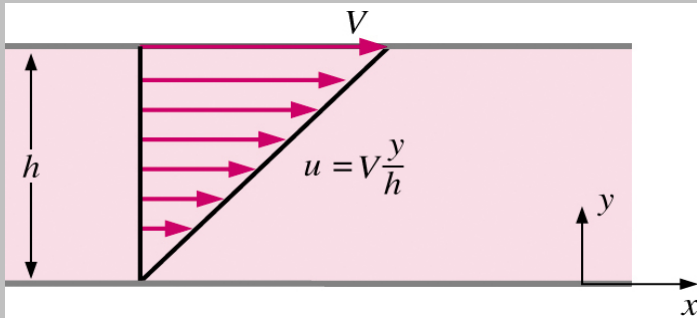
- Dynamics : $\vec{F} = m\vec{a}$

- Solid Mechanics :
$$\frac{\partial \sigma_{xx}}{\partial x} + \frac{\partial \sigma_{yx}}{\partial y} + \frac{\partial \sigma_{zx}}{\partial z} = 0$$

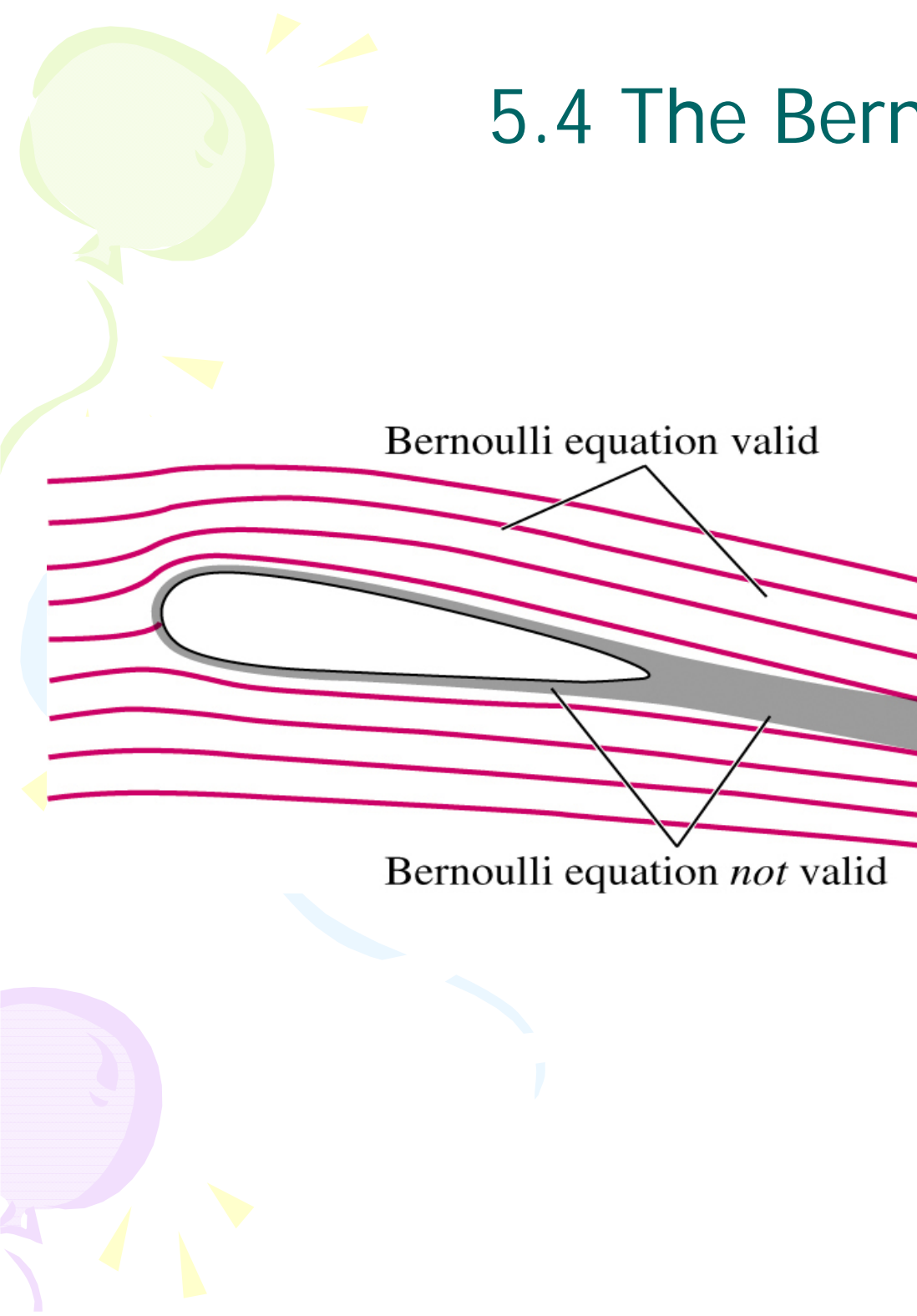
- Fluid Mechanics :
$$\rho \frac{D\vec{V}}{Dt} = -\nabla p + \rho \vec{g} + \mu \nabla^2 \vec{V}$$

What is a fluid?

- **A fluid is a substance in the gaseous or liquid form**
- **Distinction between solid and fluid?**
 - Solid: can resist an applied shear by deforming. Stress is proportional to strain
 - Fluid: deforms continuously under applied shear. Stress is proportional to strain rate

| Solid | | Fluid | |
|-------------------------------------|--|---|--|
| $\tau = \frac{F}{A} \propto \alpha$ |  |  | $\tau = \frac{F}{A} \propto \mu \frac{V}{h}$ |

5.4 The Bernoulli Equation

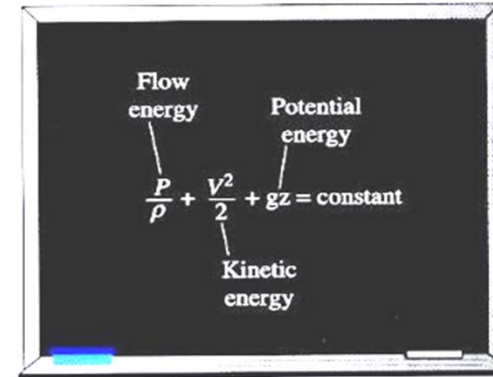


- **The Bernoulli equation is an *approximate relation between pressure, velocity, and elevation and is valid in regions of steady, incompressible flow where net frictional forces are negligible.***
- **Equation is useful in flow regions outside of boundary layers and wakes.**

5.4 The Bernoulli Equation

• Interpretation of Bernoulli Equation

- Energy point of view : Conservation of mechanical energy
- Pressure point of view : Conversion between static – dynamic – hydrostatic pressure
- Head point of view : Conversion between pressure – velocity – elevation head

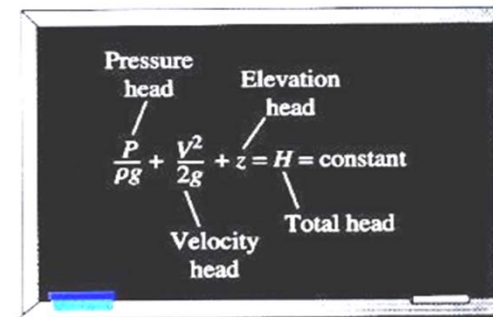


$$\frac{P}{\rho} + \frac{V^2}{2} + gz = C$$

그림 5-25

Bernoulli 방정식은 정상유동에서 유선을 따라 유체입자의 운동에너지, 위치에너지, 및 유동에너지의 합은 일정하다는 것을 나타내는 식이다.

$$P + \frac{\rho V^2}{2} + \rho g z = C$$



$$\frac{P}{\rho g} + \frac{V^2}{2g} + z = H$$

그림 5-33

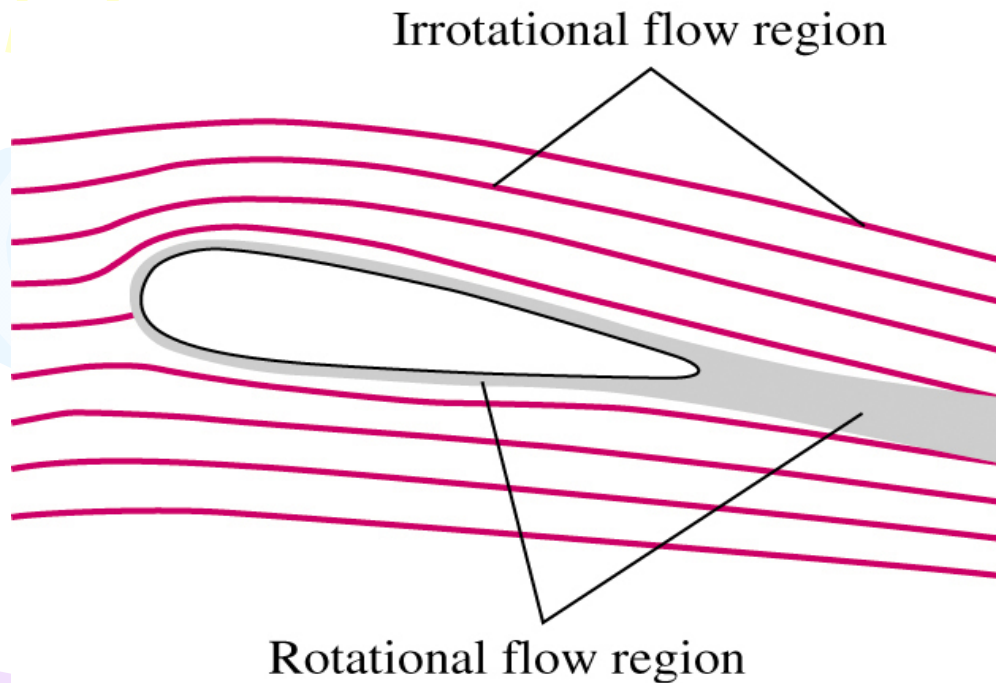
수두로 표현한 다른 형태의 Bernoulli 방정식은 다음의 의미를 갖는다: 동일한 유선을 따라 압력수두, 속도수두, 및 위치수두의 합은 일정하다.

10-5 Irrotational Flow Approximation

- **Irrotational approximation: vorticity is negligibly small**

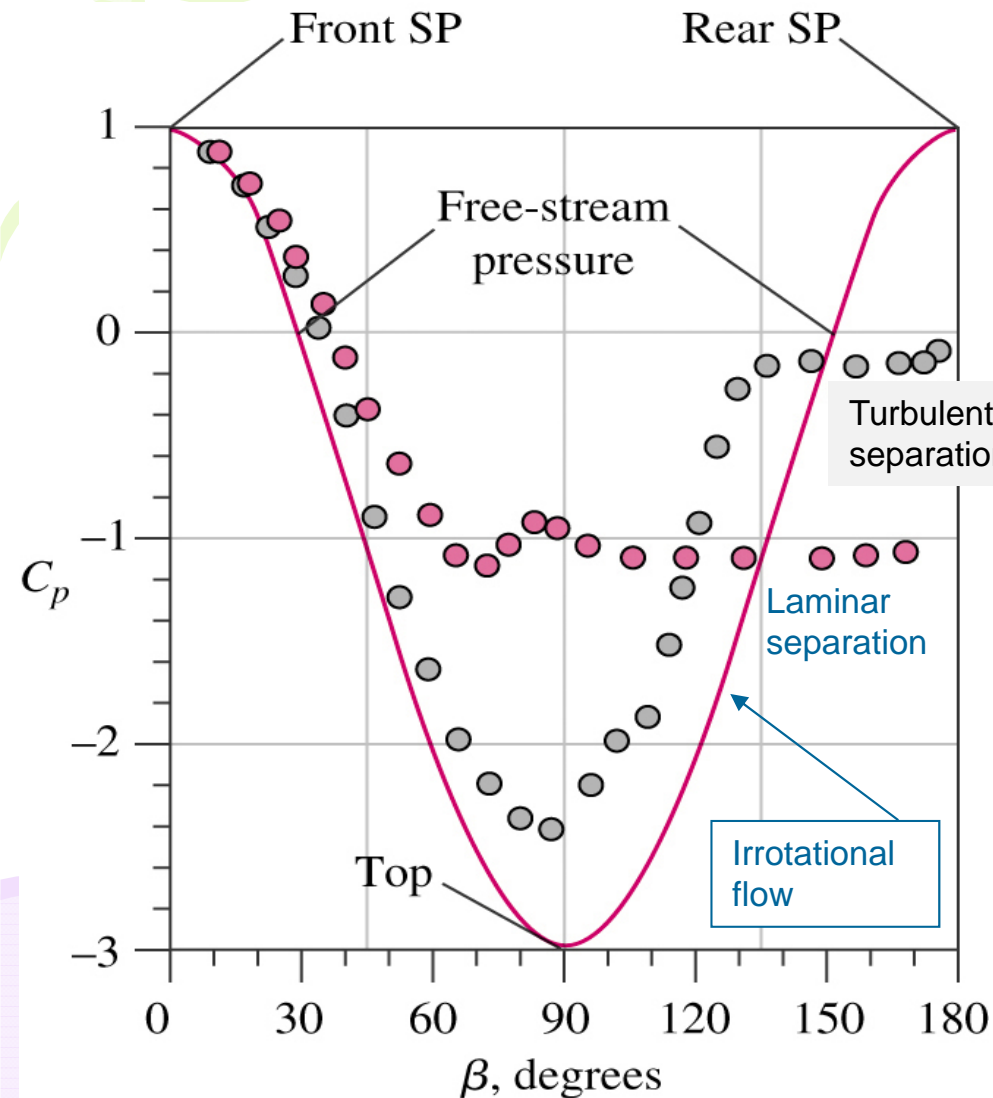
$$\vec{\zeta} = \nabla \times \vec{V} \cong 0$$

- **In general, inviscid regions are also irrotational, but there are situations where inviscid flow are rotational, e.g., solid body rotation (Ex. 10-3)**



10-5 Examples of Superposition

- **Compute pressure using Bernoulli equation and velocity on cylinder surface**



$$\frac{P}{\rho} + \frac{V^2}{2} = \frac{P_\infty}{\rho} + \frac{V_\infty^2}{2}$$

$$C_P = \frac{P - P_\infty}{\frac{1}{2}\rho V_\infty^2} = 1 - \frac{V^2}{V_\infty^2}$$

$$V^2 = U_r^2 + U_\theta^2 = 0^2 + (2V_\infty \sin \theta)^2 = 4V_\infty^2 \sin^2 \theta$$

$$C_P = 1 - 4 \sin^2 \theta = 1 - 4 \sin^2 \beta$$

$$\beta = \pi - \theta$$

10-5 Examples of Superposition

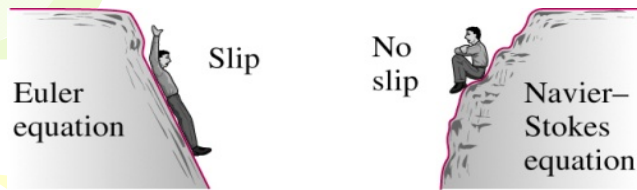
- ***D'Alembert's Paradox***: Integration of surface pressure (which is symmetric in x), reveals that the **DRAG is ZERO.** **not true !!!!**

- For the irrotational flow approximation, the drag force on **any** non-lifting body of **any** shape immersed in a uniform stream is **ZERO.**

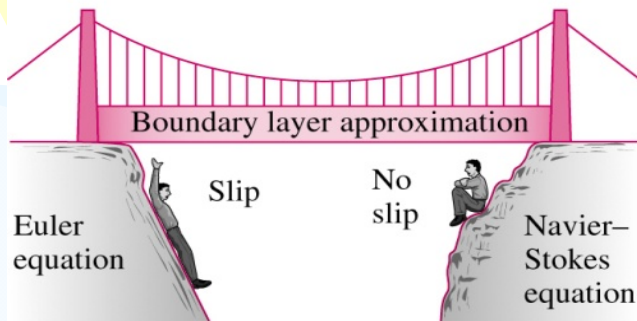
- Why?

- Viscous effects have been neglected. Viscosity and the no-slip condition are responsible for
 - Flow separation (which contributes to pressure drag)
 - Wall-shear stress (which contributes to friction drag)

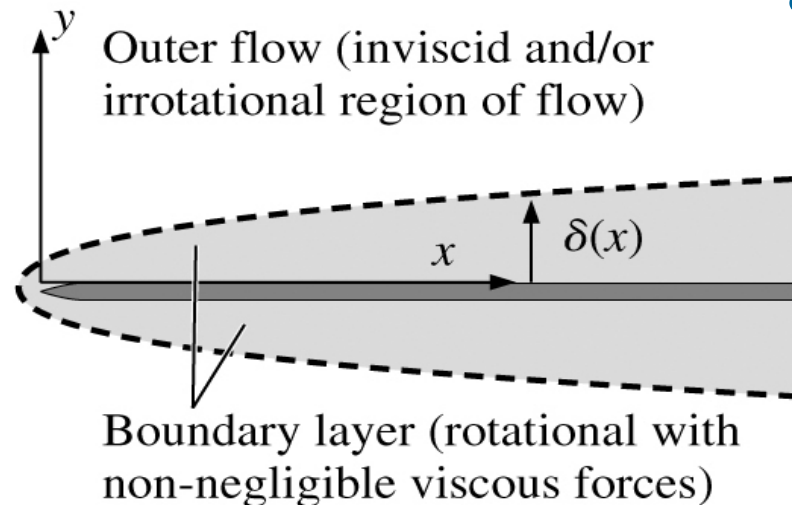
10-7 Boundary Layer (BL) Approximation



(a)



(b)

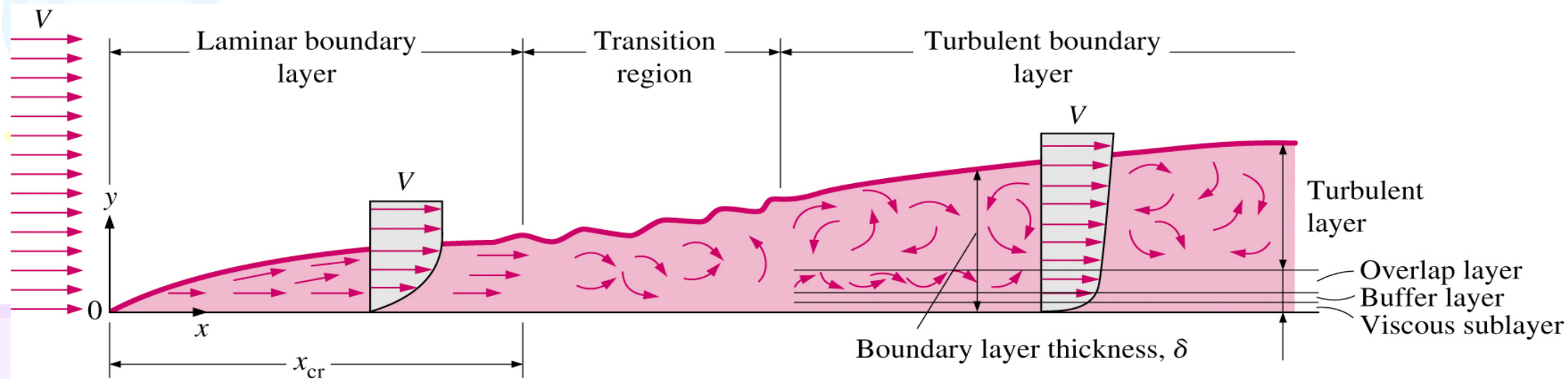


- **BL approximation bridges the gap between the Euler and NS equations, and between the slip and no-slip BC at the wall.**

- **Prandtl (1904) introduced the BL approximation**

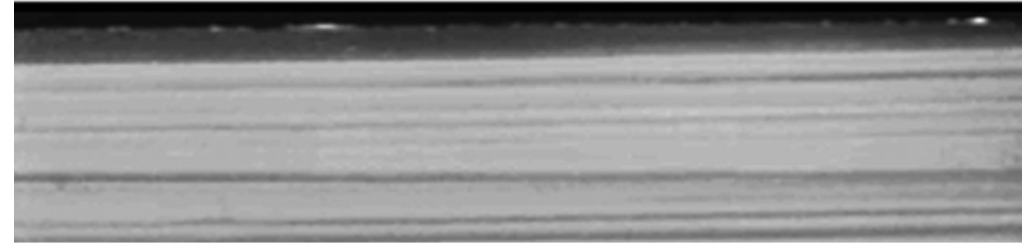
11-5 Flat Plate Drag

- Drag on flat plate is solely due to friction created by laminar, transitional, and turbulent boundary layers.**

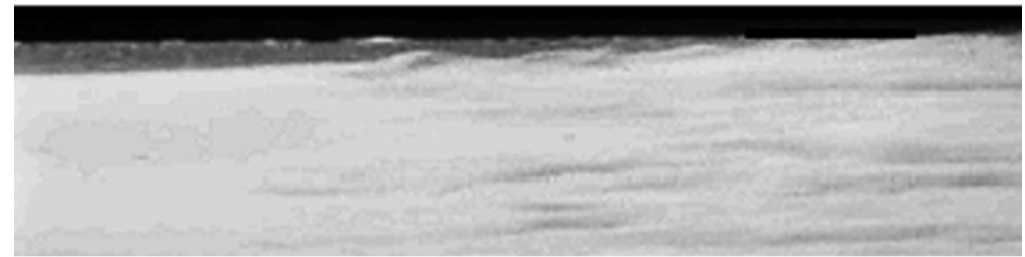


Laminar vs. Turbulent Flow

- **Laminar:** highly ordered fluid motion with smooth streamlines.
- **Turbulent:** highly disordered fluid motion characterized by velocity fluctuations and eddies.
- **Transitional:** a flow that contains both laminar and turbulent regions
- **Reynolds number, $Re = \rho UL / \mu$** is the key parameter in determining whether or not a flow is laminar or turbulent.



Laminar



Transitional



Turbulent

10-7 Pressure Gradients

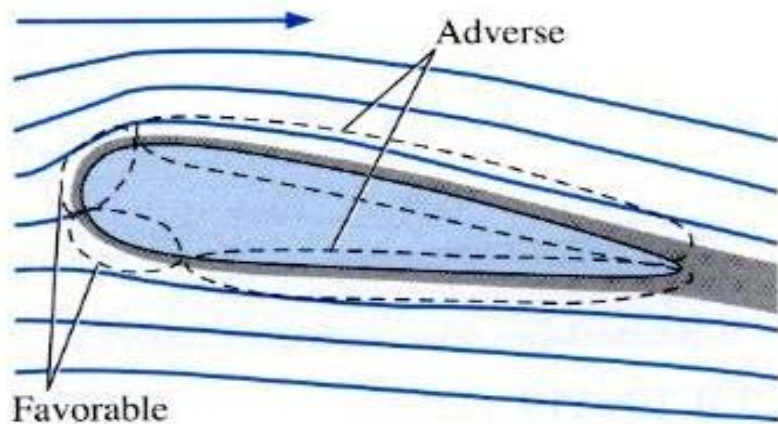
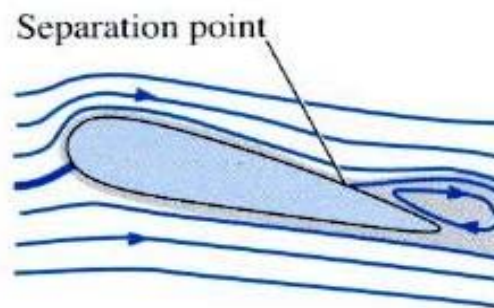
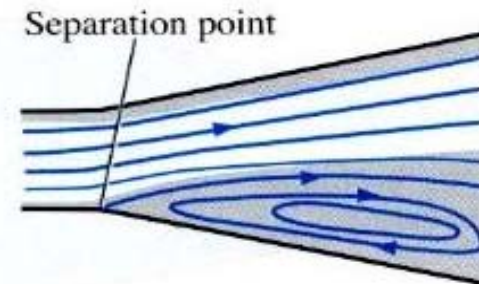


그림 10-121

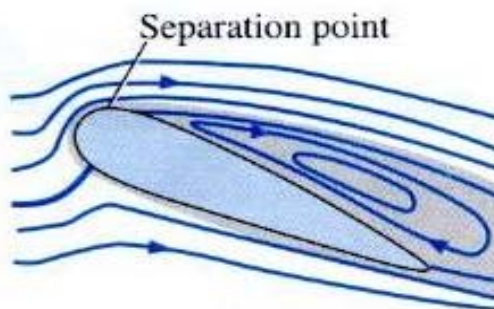
자유유동에 노출된 물체 표면을 따라 생기는 경계층에서, 앞에서는 순압력 구배, 뒤에서는 역압력 구배가 나타난다.



(a)



(c)



(b)

그림 10-122

역 압력 구간에서 박리되는 경계층의 예: (a) 일반적인 영각의 비행기 날개 (b) 높은 영각을 갖는 동일한 비행기 날개 (c) 넓은 각을 가진 디퓨저에서는 경계층이 부착되지 못하고 박리된다.

10-7 Pressure Gradients

- **Shape of the BL is strongly influenced by external pressure gradient**

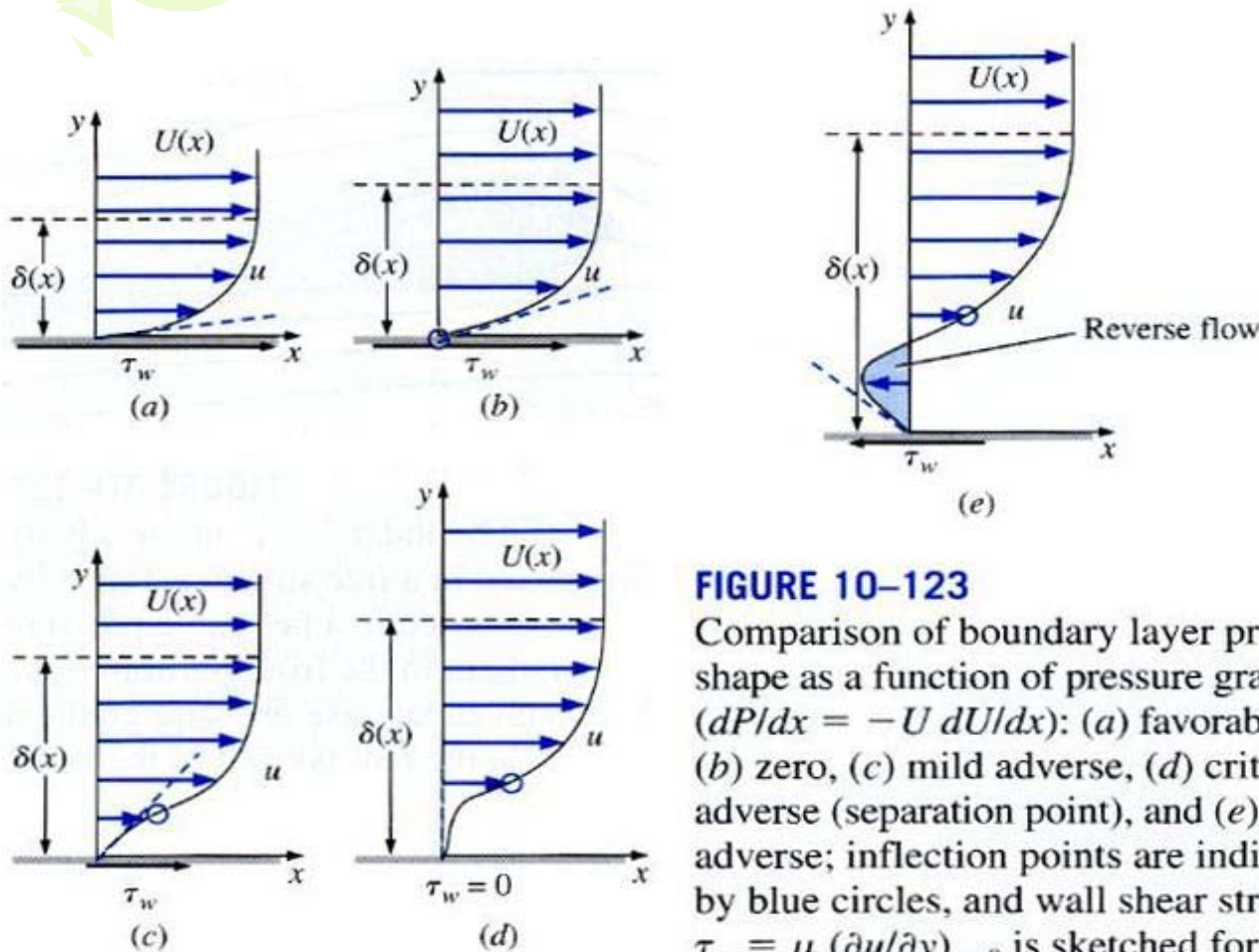
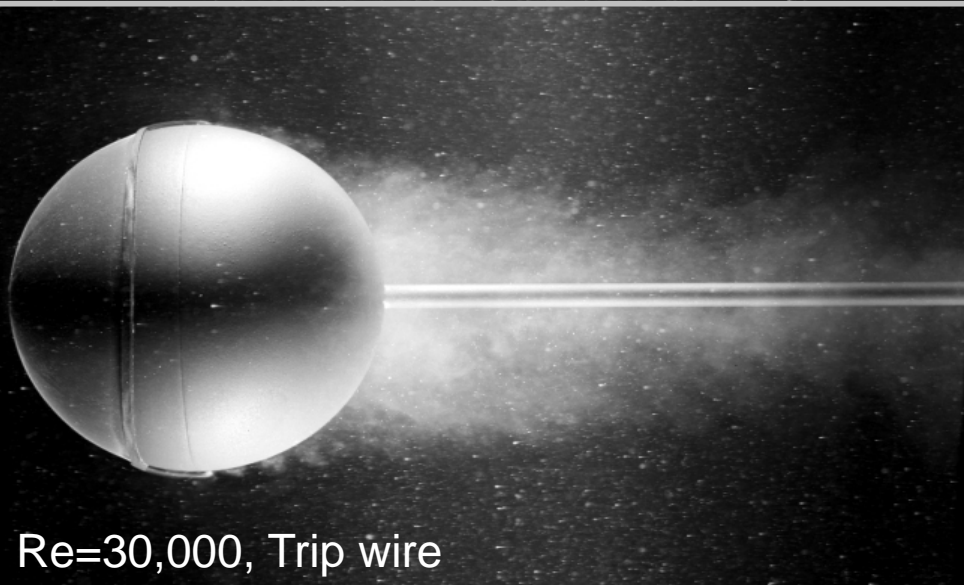
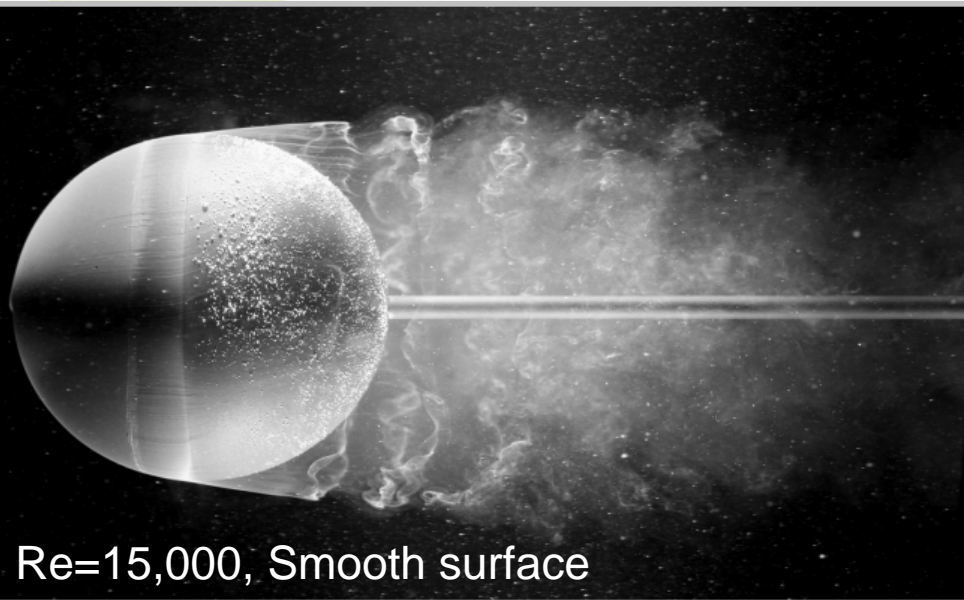


FIGURE 10-123

Comparison of boundary layer profile shape as a function of pressure gradient ($dP/dx = -U dU/dx$): (a) favorable, (b) zero, (c) mild adverse, (d) critical adverse (separation point), and (e) large adverse; inflection points are indicated by blue circles, and wall shear stress $\tau_w = \mu (\partial u / \partial y)_{y=0}$ is sketched for each case.

- (a) favorable ($dP/dx < 0$)
- (b) zero
- (c) mild adverse ($dP/dx > 0$)
- (d) critical adverse ($\tau_w = 0$)
- (e) large adverse with reverse (or separated) flow

11-6 Cylinder and Sphere Drag



- **Flow is strong function of Re.**
- **Wake narrows for turbulent flow since TBL (turbulent boundary layer) is more resistant to separation due to adverse pressure gradient.**

$$\square \theta_{\text{sep,lam}} \approx 80^\circ$$

$$\square \theta_{\text{sep,lam}} \approx 140^\circ$$

11-6 Effect of Surface Roughness

